

ALBION PROCESS™ SIMPLICITY IN LEACHING

NICKEL APPLICATIONS



ALBION PROCESS™



xstrata
technology

1 General Albion Process™ Description

The Albion Process™ is a combination of ultrafine grinding and oxidative leaching at atmospheric pressure. The feed to the Albion Process™ is a concentrate containing base or precious metals, and the Albion Process™ is used to oxidise the sulphide minerals in the concentrate and liberate these metals for recovery by conventional means.

The Albion Process™ technology was developed in 1994 by Xstrata PLC and is patented worldwide. There are three Albion Process™ plants currently in operation. Two plants treat a zinc sulphide concentrate and are located in Spain (4,000 tpa zinc metal) and Germany (18,000 tpa zinc metal). A third Albion Process™ plant is operating in the Dominican Republic treating a refractory gold/silver concentrate, producing 80,000 ounces of gold annually. A photograph of the Las Lagunas IsaMill™ and oxidative leaching circuit is shown in Figure 1. Xstrata Technology is currently completing the design and supply of an Albion Process™ plant for the GPM Gold Project in Armenia. Procurement has begun for this project, with civil works on site advanced. The GPM Gold Project will commission in September, 2013.



Figure 1
Las Lagunas Albion Plant

The first stage of the Albion Process™ is fine grinding of the concentrate. Most sulphide minerals cannot be leached under normal atmospheric pressure conditions. The process of ultrafine grinding results in a high degree of strain being introduced into the sulphide mineral lattice. As a result, the number of grain boundary fractures and lattice defects in the mineral increases by several orders of magnitude, relative to un-ground minerals. The introduction of strain lowers the activation energy for the oxidation of the sulphides, and enables leaching under atmospheric conditions. The rate of leaching is also enhanced, due to the increased mineral surface area.

Fine grinding also prevents passivation of the leaching mineral by products of the leach reaction.

Passivation occurs when leach products, such as iron oxides and elemental sulphur, precipitate on the surface of the leaching mineral. These precipitates passivate the mineral by preventing the access of chemicals to the mineral surface.

Passivation is normally complete once the precipitated layer is 2 – 3 µm thick. Ultrafine grinding of a mineral to a particle size of 80% passing 10 – 12 µm will prevent passivation, as the leaching mineral will disintegrate prior to the precipitate layer becoming thick enough to passivate the mineral. This is illustrated in Figure 2.

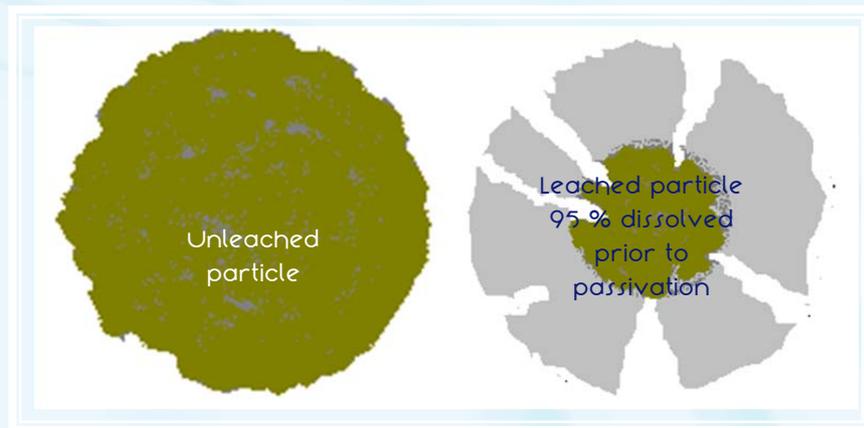


Figure 2
Mechanism of Passivation of Sulphide Minerals

After the concentrate has been finely ground, the slurry is then leached in agitated vessels, and oxygen is introduced to the leach slurry to oxidise the sulphide minerals. The agitated leaching vessels are designed by Xstrata and are known as the Albion Leach Reactor. The Albion Leach Reactor is agitated using dual hydrofoil impellers and oxygen is introduced to the leach slurry at supersonic velocity to improve mass transfer efficiency and ensure efficient oxidation of the sulphides. The Albion Leach Reactor is designed to operate at close to the boiling point of the slurry, and no cooling is required. Leaching is carried out autothermally, and the temperature of the leach slurry is set by the amount of heat released by the leaching reaction. Heat is not added to the leaching vessel from external sources, and excess heat generated from the oxidation process is removed through humidification of the vessel off gases.

2 Ultrafine Grinding and the IsaMill™ Technology

Ultrafine grinding requires a different milling action than found in a conventional ball mill, due to the fine nature of the grinding media required. In most ultrafine grinding mills, an impeller is used to impart momentum to the media charge. Media is agitated through stirring, and the resulting turbulent mixing overcomes the tendency of fine media to centrifuge. Abrasion is the major breakage mechanism in a stirred mill. The common aspects of a stirred mill are a central shaft and a series of impellers attached to the shaft. These impellers can be pins, spirals, or discs. In stirred mills, two configurations are common. In the first, the mill shaft and grinding elements are set up vertically within the mill. This type of configuration is limited in size to typically 750 kW of installed power or less. This limitation is brought about by the large break out torque imposed on the impeller located at the base of the media charge, due to the compressive load of media sitting vertically on the impeller.

In the second configuration the mill shaft is aligned horizontally within the mill chamber. This configuration, which is used in Xstrata's IsaMill™, is more cost efficient at motor sizes in excess of 500 kW. There is very little break out torque required to begin to agitate the media charge, which limits the motor size to that required for grinding only.

The IsaMill™ is a large-scale energy efficient continuous grinding technology specifically developed for rugged metalliferrous applications. Xstrata supplies the IsaMill™ technology to mining operations around the world, with over 100 mills installed in 9 countries worldwide. The IsaMill™ uses a very high energy intensity of 300kW/m³ in the grinding chamber, resulting in a small footprint and simple installation. The IsaMill™ can be scaled up directly from small scale laboratory tests. Xstrata's IsaMill™, is installed in more than two-thirds of the world's metalliferrous ultrafine grinding applications. The grinding media size for the IsaMill™ is within the size range 1.5 – 3.5 mm. Media can come from various sources, such as an autogenous media screened from the feed ore, silica sands or ceramic beads.

Xstrata will provide the IsaMill™ as a packaged Grinding Plant, consisting of the mill, slurry feed and discharge systems, media handling system, all instrumentation and control and all structural steel and platforms. Some of the IsaMill™ Grinding Plant components are shown in Figure 3 and 4. The IsaMill™ Grinding Plant incorporates all of Xstrata's operational and design experience gained from over 100 IsaMill™ installations, ensuring a trouble free commissioning.

The IsaMill™ will contain up to eight discs on the shaft, with each disc acting as a separate grinding element. The operating mechanism for the IsaMill™ is shown in Figure 5. This allows the IsaMill™ to be operated in open circuit without the need for cyclones. The IsaMill™ produces a sharp size distribution in open circuit, as the feed must pass through multiple distinct grinding zones in series before reaching the Product Separator. This plug flow action ensures no short circuiting, and efficiently directs energy to the coarser feed particles.

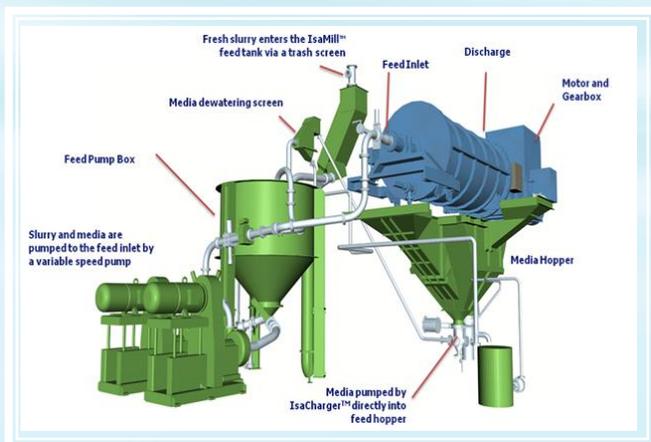


Figure 3
IsaMill™ Feed and Media Systems

passing size in the mill is typically less than 2.5 times the 80 % passing size, and very little coarse material enters the leaching circuit, resulting in very high leach recoveries.

The IsaMill™ is the highest intensity grinding technology available (>300kW/m³), meaning it is also the most compact, with a small footprint and low profile. The IsaMill™ is oriented horizontally, with the grinding plant accessed by a single platform at an elevation of approximately 3 m. Access to the mill and maintenance is simplified by the low operating aspect of the IsaMill™ and the associated grinding plant. Maintenance of the IsaMill™ is similar to routine maintenance for a slurry pump.

The Product Separator is a centrifugal separator at the end of the mill shaft that spins at sufficient rpm to generate over 20 "g" forces, and this action is responsible for the sharp classification within the mill. The IsaMill™ can be operated in open circuit at high slurry density, which is a key advantage for the leaching circuit, as the entry of water to the leach is limited, simplifying the water balance.

The IsaMill™ uses inert grinding media that produces clean, polished mineral surfaces resulting in improved leaching kinetics. A steep particle size distribution is produced in the mill. The 98 %

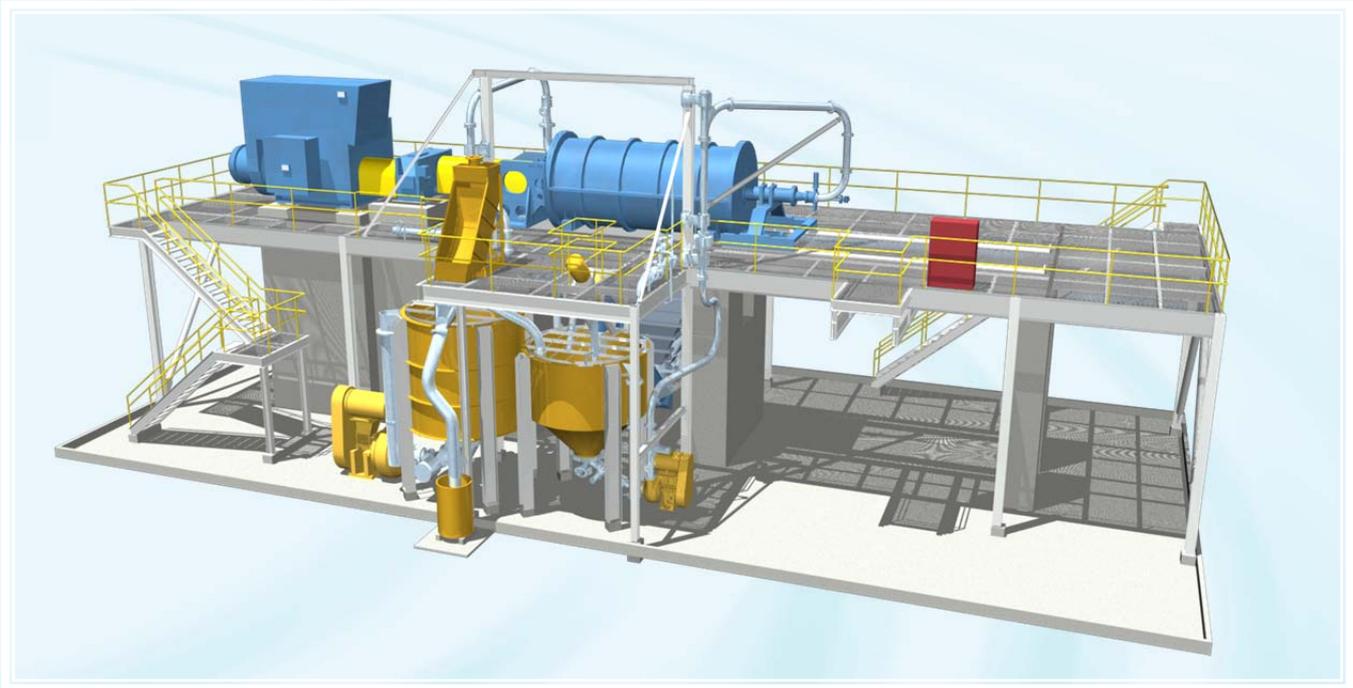


Figure 4
IsaMill™ Grinding Plant Layout

The internal rotating shaft in the IsaMill™ is counter-levered at the feed inlet end so the discharge end flange and grinding chamber can be simply unbolted and slid off using hydraulic rams. A shut down for inspection and replacement of internal wear parts takes less than 8 hours. Availability of 99% and utilisation of 96% are typical of the IsaMill™.

Scale-up of the IsaMill™ is straight forward. Laboratory test results are directly scaled to commercial size with 100% accuracy. The IsaMill™ has a proven 1:1 direct scale-up to reduce project risk.

The IsaMill™ is available in the following models:

- M500 (300 kW), capable of throughputs in the range 2 – 6 tonnes per hour
- M1000 (500 kW), capable of throughputs in the range 10 – 16 tonnes per hour
- M5000 (1200 and 1500kW), capable of throughputs in the range 20 – 60 tonnes per hour
- M10000 (3000kW), capable of throughputs in the range 60 – 100 tonnes per hour

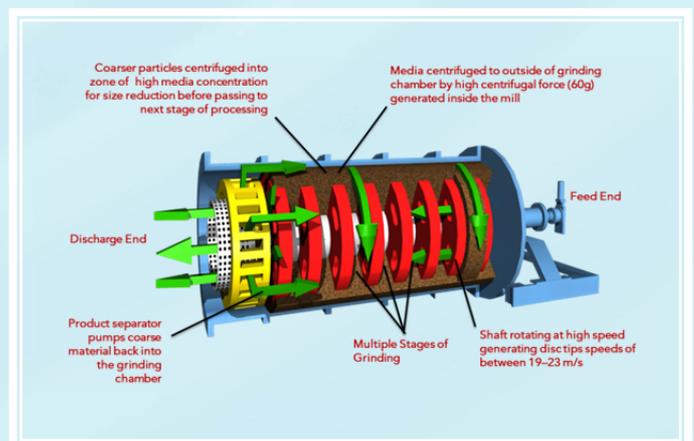


Figure 5
IsaMill™ Operating Mechanism

3 Oxidative Leaching

After the sulphide concentrate has been finely ground, it is then leached under atmospheric conditions in an oxidative leach consisting of interconnected Albion Leach Reactors. The Albion Leach Reactor is an atmospheric leaching vessel that has been designed by Xstrata Technology to achieve the oxygen mass transfer required for oxidation of the sulphide minerals at low capital and operating cost.

Oxygen is injected into the base of the Albion Leach Reactors using Xstrata's HyperSparge™ supersonic injection lances. The design of the HyperSparge™ injection system is carried out in conjunction with the design of the agitation system to ensure high oxygen mass transfer rates are achieved in the reactor. The agitator unit power is moderate, and the impeller tip speed is chosen in combination with the HyperSparge™ injection velocity to provide the required mass transfer rates.

The Albion Leach Reactor has a corrosion resistant alloy steel shell and base, supported on a ring beam or raft foundation. The tank aspect ratio is designed to achieve high oxygen transfer rates and capture efficiencies. Xstrata Technology has developed fully modular tank shell systems, which can be rapidly installed on site in one third the time of a field welded tank and at much lower costs. The Xstrata modular reactor designs require no site welding. The modular Albion Leach Reactor is shown in Figure 6.



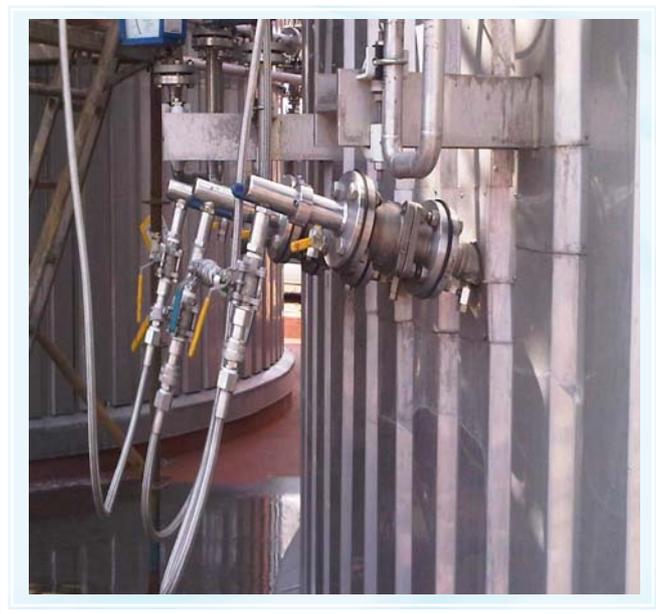
Figure 6
Albion Leach Reactor

The reactor is fitted with a centrally mounted agitator consisting of one or more hydrofoil impellers. The agitator sizing and impeller geometry is chosen by Xstrata Technology using in house correlations and testwork data to provide sufficient power to meet the oxygen mass transfer requirements in the leach vessel, as well as provide adequate solids suspension and gas dispersal. Impeller arrangements and spacing are also designed to assist in foam control within the vessel. The agitator is mounted off the tank shell, and modular maintenance platforms and structural supports are provided as part of the Albion Leach Reactor.

Key design aspects of the agitator, such as the solidity ratio, the impeller diameters and tip speeds and the overall pumping rate are determined in combination with the design of the oxygen delivery system to provide the optimum mass transfer rates in the reactor.

HyperSparge™ supersonic oxygen injection lances are mounted circumferentially around the reactor, close to the base. The HyperSparge™ is mounted externally to the tank, and penetrates through the tank wall using a series of

sealing assemblies. This design ensures that no downtime is incurred for maintenance of the oxygen delivery system, as all HyperSparge™ units can be removed live for inspection.



The HyperSparge™ injects oxygen at supersonic velocities in the range 450 – 550 m.s-1. The supersonic injection velocities result in a compressed gas jet at the tip of the sparger that incorporates slurry via shear resulting in very high mass transfer rates within the Albion Leach Reactors.

The unique design of the HyperSparge™ means that the agitator power required for the Albion Leach Reactors is much lower than is required in a conventional system. Oxygen capture efficiencies of 85 % or higher are achieved in Albion Plants within the Xstrata group using the HyperSparge™ system. A typical HyperSparge™ assembly is shown in Figure 7. The high jet velocities at the tip of the HyperSparge™ keep the nozzle clean and eliminate blockages.

The HyperSparge™ is incorporated in an overall oxygen addition and control system developed by Xstrata, consisting of in stack off gas monitoring and control of the HyperSparge™ delivery pressure. The oxygen control system is used to maintain high oxygen capture efficiencies within the Albion Leach Reactor.

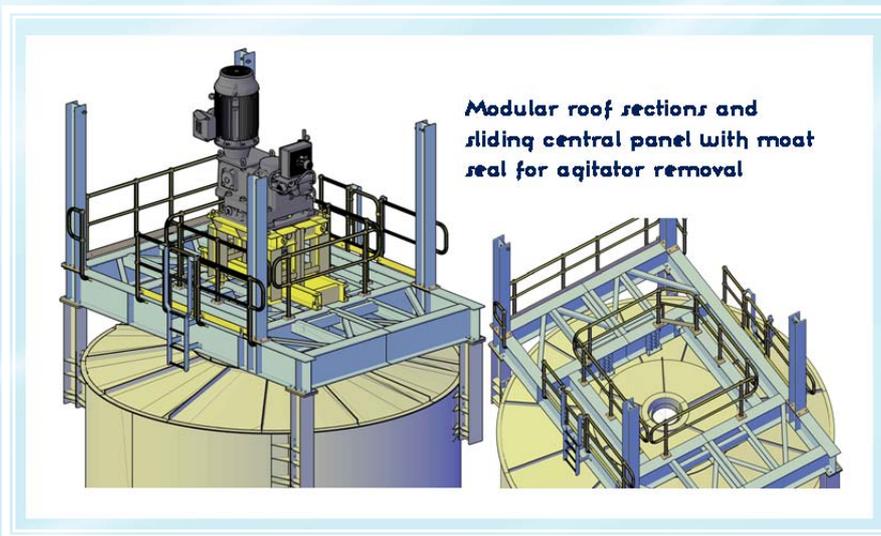


Figure 8
Albion Leach Reactor Roof Section

Exhaust gas from the oxidative leach is inert, and so the Albion Leach Reactor is fitted with sectional lids and an off gas stack to vent steam from the vessel to a safe working height. As the Albion Leach Reactors operate at close to the boiling point of the slurry, significant water vapour is released from the vessel with the exhaust gas, which assists in overall process water balance. The off gas stack is designed as a natural chimney to vent this exhaust gas to a safe working height. The exhaust gas is typically vented, however condensers can be fitted if required to recover the

evaporated water. The Albion Leach Reactor has a modular lid assembly, incorporating an agitator moat seal and sliding roof section to allow easy removal of the agitation mechanism for maintenance. This is shown in Figure 8.

Each Albion Leach Reactor has modular Internal baffles to assist mixing and prevent slurry vortexing, as well as a modular slurry riser to prevent slurry short-circuiting and assist in transport of coarser material through the leaching train.

The Albion Leach Reactors are connected in series with a launder system that allows gravity flow of the slurry through the leach train. All Albion Leach Reactors are fitted with bypass launders to allow any reactor to be removed from service for periodic maintenance. This is a low cost leaching system that is simple and flexible to operate, and the overall availability of the oxidative leach train is 99%. Xstrata Technology's launder design accommodates froth, preventing a build-up of foam in the leach train. The Launder Assembly is shown in Figure 9.

No internal heating or cooling systems are required in the Albion Leach Reactors. The vessel is allowed to operate at its equilibrium temperature, which is typically in the range 90 – 95 °C. Heat is provided by the oxidation of the sulphide minerals, with heat lost from the vessel by humidification of off gas. No direct or indirect temperature control is required, simplifying tank construction and maintenance. No external cooling towers or flash vessels are required.

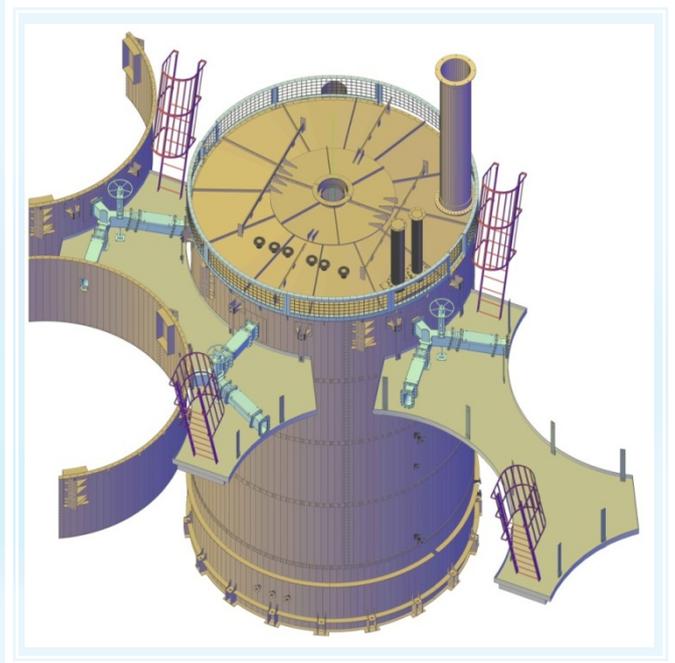
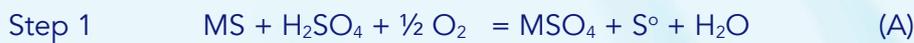


Figure 9
Launder System

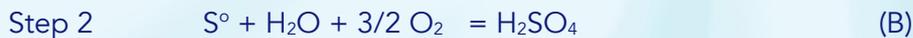
4 Oxidative Leach Chemistry

The Albion Process™ leach circuit oxidises sulphide minerals to either elemental sulphur or sulphate. This process liberates significant heat, and the oxidative leach is allowed to operate at a temperature close to the boiling point of the slurry. Typical operating temperatures are in the range 93 – 98 °C.

At these operating temperatures, mineral leaching will occur in two steps. In the first step, the mineral sulphide is oxidised to a soluble sulphate and elemental sulphur.



In the second step, the elemental sulphur is then oxidised to form sulphuric acid.



These reactions can be catalysed by the action of ferric iron under acidic conditions. The oxidative leach can be operated under a range of pH conditions, varying from acidic to neutral. The control pH will set the amount of elemental sulphur oxidation via reaction B. The extent of elemental sulphur oxidation can be varied from a few percent to full oxidation by control of the leach pH. This is the main control loop employed in the oxidative leach, with pH varied within the range 1 – 6.

Nickel and cobalt concentrates are leached under oxidising acidic conditions. Under these conditions some elemental sulphur oxidation is required to provide acid for the leach and the background acidity is held in the range 5 – 15 gpl. The leach acidity is maintained by either the addition of acid, or by allowing Reaction (B), the oxidation of elemental sulphur, to proceed. Elemental sulphur oxidation will proceed readily under the conditions found in the oxidative leach at acidities below 10 gpl, and slows significantly as the acidity approaches 15 gpl. In this way the Albion acidic leach is self regulating, oxidising elemental sulphur as required, maintaining the acidity.

The oxidative leaching of nickel-cobalt concentrates is a two stage process. The economic metals are first leached in oxygenated acidic solution, and the acidic leach slurry is then neutralised to precipitate iron and other deleterious elements such as arsenic, prior to separation of the leached solids and recovery of the nickel and cobalt metals from the neutralised leach solution. Some of the common leach reactions are outlined below. While the oxidative leach is a ferric leach, the leach reactions are presented as the oxygen equivalent to provide a better indication of reagent usage.

4.1.1 Pentlandite series

The most common of the cobalt and nickel bearing minerals are the pentlandite series. Nickeliferous and cobaltiferous pentlandite can have complex compositions, and the reactions shown below assume equimolar quantities of iron and cobalt or nickel in the mineral.

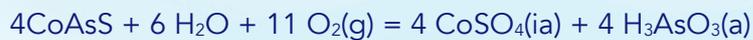




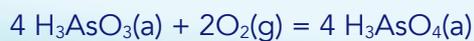
In addition to the pentlandite series, other cobalt and nickel sulphides, such as millerite, voliarite and linneite can be readily leached in the oxidative leach.

4.12 Cobaltite

Cobaltite is often present as a combination of rimming on pyrite and intimately housed within the pyrite lattice. Cobaltite will leach according to the following reaction:



In the reaction above, the arsenic liberated on oxidation of the cobaltite is shown reporting to solution as Arsenic(3⁺). Liberated arsenic can then be oxidised in the leach circuit to Arsenic(5⁺) according to the reaction:



This reaction is favoured by the presence of pyrite, as pyrite surfaces have a catalytic effect on arsenic oxidation. The extent of oxidation of Arsenic (3⁺) to Arsenic (5⁺) will depend on the leach conditions, however over 70 % of the arsenic would be expected to be present in the leach as Arsenic (5⁺).

4.13 Pyrite

Pyrite is one of the major gangue minerals present in many sulphide concentrates. The pyrite oxidation reaction in the leach will be:



Pyrite will not form elemental sulphur at leach acidities below 25 gpl, and so elemental sulphur formation is not expected from pyrite within the oxidative leach circuit. Significant pyrite leaching will not occur until most of the base metal sulphides have leached to completion, due to the galvanic effects, as pyrite is cathodically protected relative to these minerals.

4.14 Pyrrhotite

Pyrrhotite is also a common iron bearing sulphide in cobalt/nickel sulphide concentrates. Pyrrhotite will oxidise readily under the conditions found in the oxidative leach, with the formation of elemental sulphur predominating. The leach reaction for Pyrrhotite is outlined below.



In addition to the sulphide leach reactions listed above, ferric iron will be continually re-oxidised in the leach by the injection of gaseous oxygen, according to the reaction:



Elemental sulphur will also be progressively oxidised in the leach, according to the reaction:



The acid demand for the leach will be met largely by the oxidation of pyrite and elemental sulphur within the leach train. Sulphuric acid will also be added to the oxidative leach to neutralise gangue acid consumers. Sulphuric acid can be added as concentrated acid, or as acid in raffinate or spent electrolyte streams, depending on the overall process flowsheet and metal recovery circuit chosen.

4.2 Neutralisation

Both iron and sulphur, in the form of sulphates and acid will be liberated in the oxidative leach, along with minor levels of other deleterious elements such as arsenic, aluminium and silicon. On completion of the oxidative leach, the slurry will be neutralised to precipitate iron, acid and deleterious elements. Two iron precipitation circuits are commonly employed in mineral sulphide leaching circuits – Goethite and Jarosite.

The neutralisation circuit will be operated using the same Albion Leach Reactors as used in the oxidative leaching circuit, to ensure commonality of spares and simpler maintenance. The intertank launder system will be the same as employed in the oxidative leach, and all reagent mains will have dosing points extending through the interface between the leach and neutralisation stages. This will allow several tanks to be operated as either leach or neutralisation vessels, providing flexibility for differing concentrate compositions.

A goethite based circuit is described below, however Xstrata has operational experience in both goethite and jarosite circuits. When the neutralisation stage is operated as a goethite circuit, the following key control parameters are set:

- Ferric levels in all tanks are maintained at less than 1 g/L at all times and the temperature is maintained at over 85 degrees. This ensures that iron precipitates as goethite, and any arsenic as a stable ferric arsenate.
- The circuit is operated with precipitated solids recycle to partially neutralise acid exiting the leach train and provide seed to the neutralisation circuit. This enhances crystal growth at the expense of nucleation, and improves the settling and filtration properties of the precipitate.

- The pH profile across the neutralisation circuit is progressively increased in discrete steps to minimise supersaturation of both iron and sulphate in the neutralised solution. This ensures a stable crystalline precipitate and minimises nucleation and scale formation.

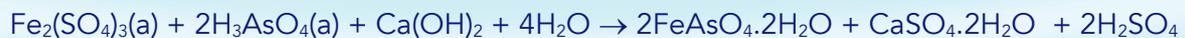
The oxidative leach discharge slurry is initially neutralised to a pH of 1.8 – 2.2 in the first neutralisation reactor, by adding recycled neutralised product. The pH is then increased in the subsequent neutralisation vessels to 3.5 - 4, with oxygen added to assist ferrous oxidation to ferric. Cobalt and nickel will not precipitate from solution at this terminal pH, however iron removal will be complete. Any residual ferrous iron present in the leach discharge will be oxidised at the more neutral pH to ferric iron.

Ferric iron will then be precipitated as goethite:



Goethite and the analogous phase, ferrihydrite, will be the favoured iron precipitates in the neutralisation stage, due to the operating temperature of approximately 85-95°C. Minor hematite formation will also occur.

Iron will co-precipitate with arsenic in the neutralisation stage according to the reaction:



Arsenic will be fixed in the residue as ferric arsenate. To ensure a stable ferric arsenate is formed, the neutralisation circuit operating conditions must favour precipitation of ferric arsenate through growth onto existing particles of crystalline ferric arsenate over nucleation and precipitation of amorphous iron arsenic phases. These considerations are taken into account in the design of the neutralisation circuit, and some of these key principles were outlined earlier.

Either oxygen or air can be used as the oxygen source in the neutralisation stage. Oxygen is recommended to promote the iron and arsenic oxidation kinetics and to prevent excess heat loss due to humidification of off-gas. High temperatures in the neutralisation circuit are important in forming a stable arsenic precipitate.

5 Process Flowsheet –Nickel/Cobalt Concentrates

A flowsheet for the Albion Process™ for nickel-cobalt concentrates is shown in Figure 10. Following the Albion Process™, there are several options available for nickel recovery from the final solution, including the following:

- Nickel and cobalt recovery as a mixed hydroxide for sale or further refining
- Nickel and cobalt recovery as a mixed sulphide for sale or further refining
- Nickel and cobalt recovery by solvent extraction and electrowinning

The current flowsheet outlines nickel recovery as a mixed hydroxide precipitate, however Xstrata Technology would study the best nickel and cobalt recovery methods for the client once the composition of the concentrate is better understood. Xstrata is the world's third largest producer of nickel and cobalt and operates the world's largest cobalt and nickel solvent extraction and electrowinning plants at its Nikkelverk refinery in Norway.

A bulk sulphide concentrate containing nickel, cobalt and potentially platinum group metals would be delivered as slurry to the Albion Process™ Plant. The slurry would be thickened prior to delivery, to 45 % w/w solids. The Albion Process™ does not require a high grade concentrate, and a rougher concentrate is suitable for feed to the leach. Slurry would be milled in an IsaMill™ circuit to an 80 % passing size of 10 – 12 microns prior to transfer to the oxidative leaching circuit. The IsaMill™ would operate in open circuit.

The slurry would then be oxidised in the oxidative leaching circuit in a series of Albion Leach Reactors. The reactors would operate at a temperature in the range 90 – 96 °C, with a residence time of 24 hours. Cobalt and nickel recovery to the leach solution would be over 98 %. The level of oxidation will be sufficient to liberate the cobalt, nickel, precious and platinum group metals. Acid would be dosed to the leach as required to maintain the acidity in the range 5 – 8 gpl.

The oxidised slurry would then be neutralised to a pH of 3.5 with limestone slurry to remove iron and aluminium. Neutralisation would precipitate iron as goethite, aluminium as alunite and acid as gypsum. The neutralised slurry would be filtered, and the filtrate directed to the nickel recovery circuit.

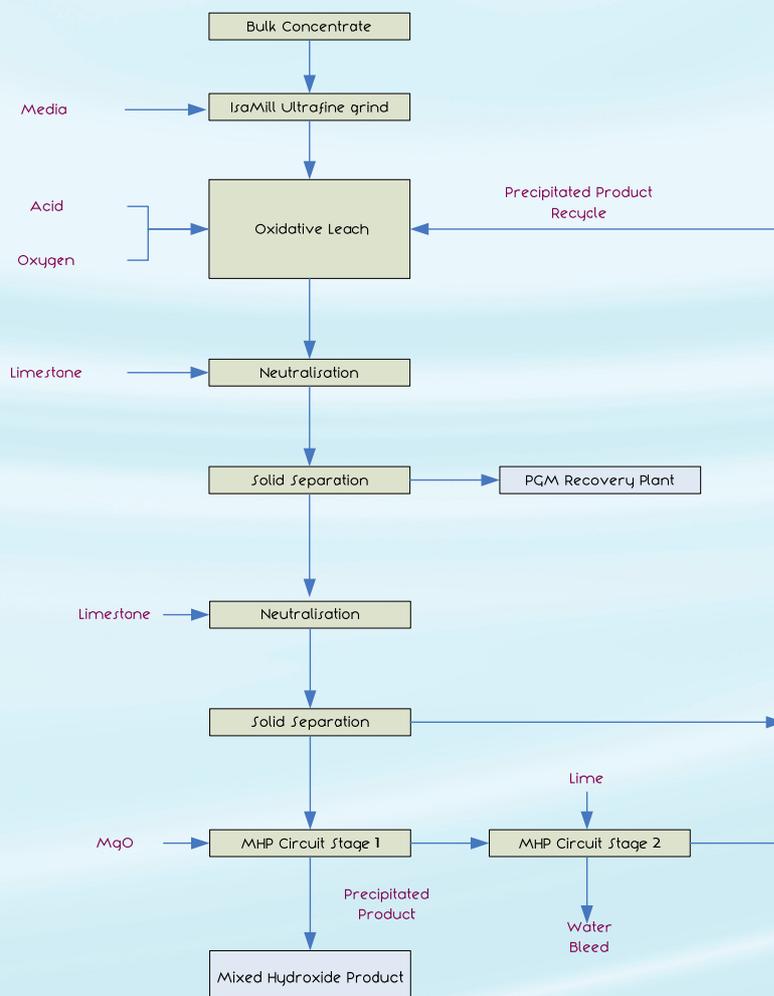
Neutralised filter cake would be re-pulped and transferred to a dedicated plant for recovery of the precious metals and platinum group metals. No precious metals and platinum group metals will be soluble in the acid sulphate leach liquor and will all report to the oxidised residue.

The solution from the neutralisation stage may require additional purification, depending on the composition of the concentrate. In the flowsheet described, it has been assumed that further purification is not required prior to nickel recovery, and solution from the neutralisation stage would be transferred to a mixed hydroxide precipitation stage using magnesium oxide to precipitate a mixed nickel/cobalt hydroxide for filtration and sale. Recycled mixed nickel/cobalt hydroxide product would also be added to the precipitation vessels to act as seed.

Approximately 80 – 90 % of the nickel and cobalt would be recovered to the mixed nickel/cobalt hydroxide product, with the remainder left in solution for recycle to the leach. This will ensure a high grade mixed nickel/cobalt hydroxide product.

Filtrate from the magnesium oxide precipitation stage will be treated with lime slurry to recover residual economic metals, with the precipitate recycled to the oxidative leach circuit. The solution phase after lime precipitation would then be returned to general process water to bleed magnesium from the Albion Process™ Plant.

Figure 10
Flowsheet for the Treatment of Nickel-Cobalt Concentrates using the Albion Process™



6 Engineering and Project Development Services

Xstrata Technology is the developer and owner of the Albion Process™ technology and offers the technology to clients worldwide.

Xstrata Technology provides lump sum equipment design and supply packages to all Albion Process™ clients. The scope of supply includes the full Albion Process™ plant, inclusive of all structural steel, piping and launders, platforms, stairways and support structures. Full civil and foundation design can be included in the Xstrata Technology scope of work. Construction is supplied by the client, with supervisory labour provided by Xstrata.

The Albion Process plant package provided by Xstrata Technology is low cost and low risk, and incorporates all of Xstrata's knowhow in the 20 year development history of the IsaMill™ and Albion Process™ technologies. Xstrata Technology can work with our client's EPCM contractor to ensure that the Albion Process™ plant interfaces with all other plant areas in an efficient manner.

Xstrata Technology involvement in a project usually begins at the testwork stage, with a testwork and project development program designed for the client by Xstrata and our marketing partner Core Resources. All testwork is carried out at an approved testing facility. Xstrata can provide a range of Engineering Studies in support of the testwork programs to provide capital and operating cost data for the Albion Process™ plant. Xstrata Technology can also provide Feasibility Study services, ultimately leading to a lump sum equipment design and supply package, which is fully guaranteed by Xstrata.

As an introduction to the Albion Process™ technology, Xstrata can provide desktop capital and operating cost estimates for an Albion Process™ plant at no cost to our clients, once provided with a concentrate composition and planned throughput.

For more information on the Albion Process™, please refer all enquiries to:

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Tough testing grounds that make our process technologies the best on earth.

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